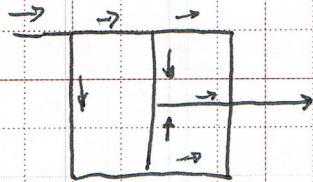


DETAILS

ENGINEERING & CONSULTING

P.17-23

31. PIPE NETWORK, MULTI-LOOP, HARDY CROSS



$$\sum Q_{in} = \sum Q_{out}$$

$$\sum HL (\text{ANY CLOSED LOOP}) = 0$$

friction loss in a Run is $h_f = K' Q^n$

$n=2$	DARCY
$n=1.85$	H.W.

$D, L, ft; Q, ft^3/sec$ $K' = 0.02517 \frac{fL}{D^5}$ DARCY

$K' = 4.727 \frac{L}{D^{4.8655}}$ H.W.

$D^{4.8655} \cdot C^{1.85}$

OTHER UNITS AVAILABLE

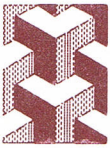
$$Q = Q_{assumed} + S_{CORRECTION}$$

$$S = - \frac{\sum h_f}{n \sum h_f / Q^n}$$

Same for all Pipes in one Loop

Hardy Cross

- 1) $n=2$ (DARCY); 1.85 H.W.
- 2) POSITIVE: CLOCKWISE
- 3) Label All branches in Network
- 4) Separate All LOOPS that each Branch is in the LOOP
- 5) CALC. K' for each Branch
- 6) ASSUME REASONABLE Q & DIRECTION FOR EACH BRANCH
- 7) CAL. S FOR EACH LOOP
- 8) APPLY S TO each BRANCH
- 9) Repeat 7 \rightarrow 8, 9



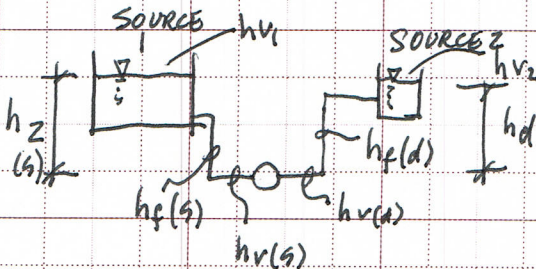
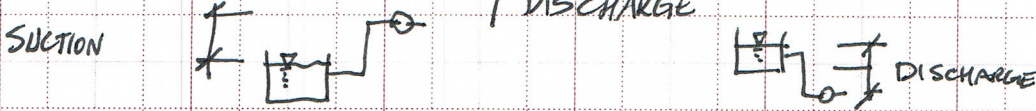
P.18-6 HYDRAULIC MACHINES

$$h = \frac{P}{\gamma} = \frac{P}{\rho g} \text{ (SI)} = \frac{P}{\rho} \left(\frac{gc}{g} \right) \text{ US.}$$

$$h_f = \frac{fLV^2}{2Dg} \text{ friction head}$$

$$h_{rv} = \frac{V^2}{2g} \text{ dynamic head}$$

$$h_z = \text{static head}$$



TOTAL STATIC $h_t(s) = h_p(s) + h_v(s)$
@ PUMP INLET.

$$h_t(s) = h_p(i) + h_z(s) + h_v(i) - h_f(s)$$

(PRESSURE) (VELOCITY)
(FRICTION) (VELOCITY @)

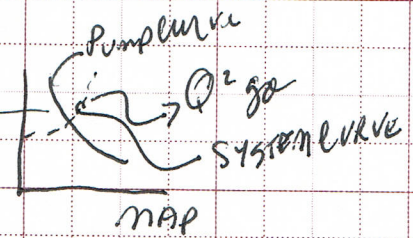
$$h_z + h_d + h_{pump} = h_{fs} + h_{fd}$$

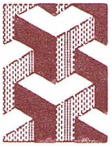
$$h_{pump} = (h_d - h_z) + h_{fs} + h_{fd} \rightarrow \frac{Q^2}{A^2} \frac{fD}{2Dg} = \frac{Q^2}{A^2} \frac{fD}{2g}$$

$$Z_1 + h_{pump} = Z_2 + \frac{fL_1}{D_1} \frac{V_1^2}{2g} + \frac{fL_2}{D_2} \frac{V_2^2}{2g}$$

$$h = a + bQ^2$$

Solve pump PROBLEM Graph





DETAILS

ENGINEERING & CONSULTING

P.18-18
a) AFFINITY LAWS

$$\frac{Q_2}{Q_1} = \frac{n_2}{n_1}$$

$$\frac{h_2}{h_1} = \left(\frac{n_2}{n_1}\right)^2 = \left(\frac{Q_2}{Q_1}\right)^2$$

Power

$$\frac{P_2}{P_1} = \left(\frac{n_2}{n_1}\right)^3 = \left(\frac{Q_2}{Q_1}\right)^3$$

IMPELLER DIAM. = CONS.
SPEED IS VARIED

b) SPEED CONSTANT / IMPELLER IS VARIED

$$\frac{Q_2}{Q_1} = \frac{D_2}{D_1}$$

$$\frac{h_2}{h_1} = \left(\frac{D_2}{D_1}\right)^2$$

$$\frac{P_2}{P_1} = \left(\frac{D_2}{D_1}\right)^3$$

PUMP SIMILARITIES: (DYNAMICALLY SIMILAR)

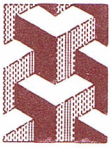
$$\frac{n_1 D_1}{\sqrt{h_1}} = \frac{n_2 D_2}{\sqrt{h_2}} \quad \frac{Q_1}{D_1^2 \sqrt{n_1}} = \frac{Q_2}{D_2^2 \sqrt{n_2}}$$

$$\frac{P_1}{\rho D_1^2 h_1^{1.5}} = \frac{P_2}{\rho D_2^2 h_2^{1.5}}; \quad \frac{Q_1}{n_1 D_1^3} = \frac{Q_2}{n_2 D_2^3}; \quad \frac{P_1}{\rho n_1^3 D_1^5} = \frac{P_2}{\rho n_2^3 D_2^5}; \quad \frac{n_1 \sqrt{Q_1}}{(h_1)^{0.75}} = \frac{n_2 \sqrt{Q_2}}{(h_2)^{0.75}}$$

ASSUME: TURBULENT Region

Same Pump Eff.

Same % of wide open flow



DETAILS

ENGINEERING & CONSULTING

510-1
1)

$$\frac{1}{4} \pi D^2 = 0.2083$$

$$\frac{D}{2} = 0.2083 \quad L = 0.104$$

$$Q = VA = 1.318 C A R^{0.63} S^{0.54}$$

C = 100 OR LOOKUP

$$S^{0.54} = 0.03738 Q$$

$$S = 0.002273 Q^{1.8159}$$

NO
R. HYDRAULIC
RADII

$$h_f = L * S = (3000) S$$

R = $\frac{TD^2}{4}$ / TD
AREA = $\frac{D^2}{4}$
Pump

$$\begin{aligned} \text{TDH (TOTAL DYNAMIC HEAD)} &= \Delta H_f + h_f + \frac{V^2}{2g} \\ &= 560.530 + (3000)(0.002273) Q^{1.8159} + \frac{V^2}{2g} \end{aligned}$$

$$V = Q/A$$

$$\text{TDH} = f(Q, Q^2)$$

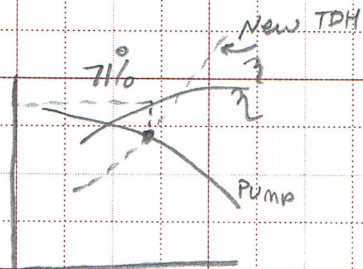
3) IF PIPE \rightarrow 8" @ New Point of OPERATION

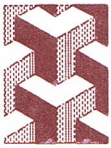
$$Q = VA = 1.318 C A R^{0.63} S^{0.54}$$

$V = Q/A$
 $\frac{1}{4} \pi D^2 = (0.12) = 0.349 \text{ ft}^2$
 $S = f(Q, Q^2)$
 $\frac{D}{4} =$

$$S^{0.54} = \frac{Q}{1.318 C A R^{0.63}} = 0.06721 Q$$

TDH VS Q
X PUMP & SYSTEM
UP TO η CURVE





DETAILS

ENGINEERING & CONSULTING

AN AVERAGE ANNUAL DISCHARGE RECORD FOR A RIVER COVERS A PERIOD OF 83YR. THE AVERAGE FLOW DURING THE ENTIRE PERIOD OF RECORD WAS 1947 FT³/SEC WITH A STD DEVIATION OF 613 FT³/SEC. WHAT IS THE AVERAGE FLOW WILL PRODUCE THE 50-YEAR FLOOD?

USE GUMBEL DISTRIBUTION COEFFICIENT (GDC) CHARTS

K ₅₀	GDC FOR 50YR RECORD	≠ 50YR FLOOD	= 2.89
K ₈₃	" " 83 " "	≠ 50 " "	= ?
K ₁₀₀	" " 100 " "	≠ 50 " "	= 2.77
n	YEARS OF RECORD		= 83

USE INTERPOLATION $K_{83} = K_{50} + \frac{(K_{100} - K_{50})(n - 50)}{100 - 50}$

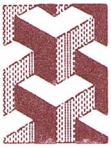
$$= 2.89 + \frac{2.77 - 2.89}{100 - 50} (83 - 50) =$$

$$K_{83} = 2.89 + (2.77 - 2.89) \frac{(83 - 50)}{(100 - 50)} = 2.81$$

$Q_p = \text{FLOWRATE FOR THE PERIOD OF INTEREST} = Q_m + K_{83} \sigma$
 $(Q_m = \text{AVERAGE FLOW RATE ; } \sigma = \text{STD DEV.}) = 1947 + (2.81)(613)$
 $= \underline{\underline{3670 \text{ FT}^3/\text{SEC}}}$

CANNOT DO & USE:

- SIMPLE RATIO $\frac{QP}{50} = \frac{1947}{83}$ $QP = 1173 (1200)$ No use of σ
- INCORRECT READING OF GUMBEL CHARTS.
RETURN PERIOD VS. RECORD OF LENGTH



DETAILS

ENGINEERING & CONSULTING

250 mL WATER SAMPLE WITH AN INITIAL pH OF 9.7 IS TITRATED WITH 0.03 N H_2SO_4 . A pH OF 8.3 IS REACHED AFTER 6 mL OF ACID ARE ADDED & A pH OF 4.5 IS REACHED AFTER 12 mL OF ACID ARE ADDED. WHICH ALKALINITY SPECIE DOMINATES & WHAT IS ITS CONCENTRATION?

FIRST FIND OUT, HOW DOES INITIAL pH INFLUENCE DISTRIBUTION OF ALKALINITY SPECIES? pH OF 9.7, DOMINATE ALKALINITY = CARBONATE

FOR HYDROXIDE ALKALINITY pH=9.7; pH+pOH=14; pOH=14-9.7=4.3

$[OH^-]$ = HYDROXIDE CONCENTRATION mol/L

pOH = $-\log [OH^-]$ $[OH^-] = (10^{-4.3})$ mol/L

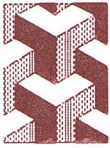
(EW) CALCIUM CARBONATE EQUIV. WT 50,000 mg/eq

(OH)⁻alk HYDROXIDE ALKALINITY mg/L as CaCO₃

(V)alk VALENCE eq/mol

$$OH^-_{alk} = [OH^-] / V / EW = 10^{-4.3} \frac{\text{mol}}{\text{L}} \left(\frac{1 \text{ eq}}{\text{mol}} \right) \left(\frac{50,000 \text{ mg CaCO}_3}{\text{eq}} \right)$$

$$= 2.5 \text{ mg/L as CaCO}_3$$



DETAILS

ENGINEERING & CONSULTING

SPILLWAY 2.5m WIDE & HYDRAULIC JUMP OCCURS AT TOE. WATER DEPTH OF 0.15m & $Q = 2.93 \text{ m}^3/\text{s}$. WHAT IS TOTAL HEAD DISSIPATED.

V_1, Q, d_1, W
 V_2, Q, d_2, W

BEFORE HYDRAULIC JUMP
AFTER HYDRAULIC JUMP

$$V_1 = Q/d_1 W = 2.93 \text{ m}^3/\text{s} / ((0.15 \text{ m}) 2.5 \text{ m}) = 7.8 \text{ m/s}$$

$$\text{CONJUGATE DEPTH: } d_2 = -0.5 d_1 + \sqrt{\frac{2V_1^2 d_1}{g} + 0.25 d_1^2}$$

$$= -0.5(0.15) + \left[\frac{2(7.8)^2 (0.15)}{9.8} + 0.25(0.15)^2 \right]^{1/2}$$

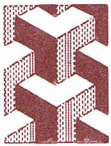
$$V_2 = Q/d_2 W = 2.93 \text{ m}^3/\text{s} / [1.29 (2.5) \text{ m}^2] = 0.91 \text{ m/s}$$

$d_2 = 1.29 \text{ m}$
 $V_2 = 0.91 \text{ m/s}$

$$H_1 + \frac{V_1^2}{2g} + d_1 = H_2 + \frac{V_2^2}{2g} + d_2$$

$$\Delta H = H_2 - H_1 = \frac{V_1^2}{2g} + d_1 - d_2 - \frac{V_2^2}{2g} = d_1 - d_2 + \frac{1}{2g} (V_1^2 - V_2^2)$$

$$= (0.15 - 1.29) + \frac{1}{(9.81)} \left(\frac{7.8^2 - 0.91^2}{2} \right) = 1.92 \text{ m HEAD ENERGY}$$



DETAILS

ENGINEERING & CONSULTING

CULVERT (1m HIGH, 27m LONG, 2% SLOPE, 1202.83m UPSTREAM SURFACE ELEVATION, & 1202.38m DOWNSTREAM SURFACE ELEVATION) INVERT ELEVATION OF THE CULVERT OUTLET IS 1201.17m. WHAT IS THE CULVERT FLOW CLASSIFICATION?

SLOPE OF CULVERT, 2%

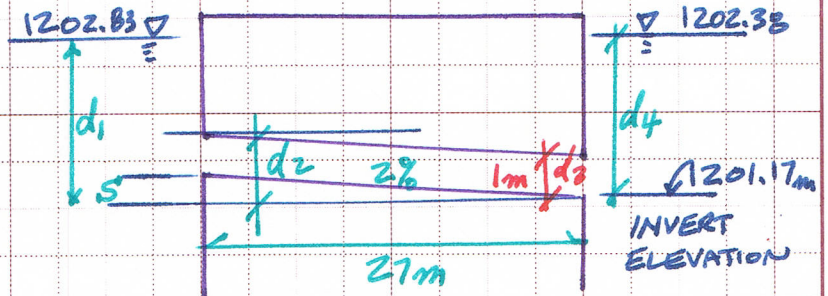
$$S = \frac{L}{S} = (27)(0.02) = 0.54m$$

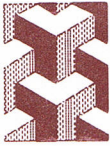
$$d_1 = 1202.83 - 1201.17 = 1.66m$$

$$d_2 = S + \text{DIAMETER} = S + d_3 = 1.0 + 0.54 = 1.54m$$

$$d_4 = 1202.38 - 1201.17 = 1.21m > d_3 = 1.0m \text{ by } 0.21m \text{ SUBMERGED.}$$

SUBMERGED INLET & OUTLET IS TYPE 4





DETAILS

ENGINEERING & CONSULTING

RECTANGULAR CHANNEL WITH 8m BASE, 1.5m WATER DEPTH, VELOCITY = 2.5m/s TRANSITIONS TO A CIRCULAR CULVERT 50m UNDER A HIGHWAY. CONCRETE BASE & SLOPE OF 0.002m/m USED. WHAT IS THE REQUIRED CULVERT CONCRETE STANDARD PIPE WITH HALF FULL? USE MULTIPLES OF 9' OR 8' PIPES.

FOR 1/2 FULL $\theta = \pi = 180^\circ$

$$R_{\text{HYDRAULIC RADIUS}} = 0.25 \left(1 - \frac{\sin \theta}{\theta}\right) D$$

$$= 0.25 \left(1 - \frac{\sin \pi}{\pi}\right) D = 0.25 D$$

DEPTH IN CULVERT = $d_2 = D/2 \rightarrow D = 2d_2$

1/2 CONCRETE PIPE (MANNING) = $R^{2/3} \sqrt{S} / n = R^{2/3} \sqrt{0.002} / 0.013$

$$R = 0.25 D = (0.25) 2d_2 = 0.5d_2$$

$$= (0.5d_2)^{2/3} \sqrt{0.002} / 0.013 = 2.167 d_2^{2/3} \text{ m/s}$$

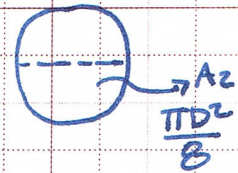
Channel $V_1 A_1 = V_2 A_2$ CULVERT

$$V_1 A_1 = (1.5) V_1 = (1.5) 8 (2.5) = 30 \text{ m}^3/\text{s} = A_2 V_2$$

$$= V_2 \frac{\pi D^2}{4} = V_2 \frac{\pi 4d_2^2}{4}$$

$$= V_2 \frac{\pi}{2} d_2^2$$

$$= (2.167 d_2^{2/3}) \frac{\pi}{2} d_2^2$$



$$30 \text{ m}^3/\text{s} = Q = 3.4 d_2^{8/3} \text{ m}^3/\text{s} \rightarrow d_2 = 2.26 \text{ m}$$

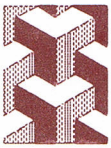
$$D = 4.5 \text{ m} = 15 \text{ FE}$$

TRY 3 PIPES: $\frac{\pi D^2}{4} / 3 = \frac{\pi 15^2}{4} / 3$ OR $\frac{\pi D^2}{4} / 3 = \frac{\pi (4.5)^2}{4} / 3 = 5.3 \text{ m}^2$

$$D_{\text{PER PIPE}} = \sqrt{\frac{4A}{\pi}} = \left[\frac{4(5.3)}{\pi} \right]^{1/2} = 2.6 \text{ m} = 8.5 \text{ FE}$$

NOMINAL PIPES = 9 FE

TYPICAL OF 3.



DETAILS

ENGINEERING & CONSULTING

A 3 IN SCH. 40 PIPE WITH 90° ELBOWS IS POSITIONED NO DIAMETER CHANGE OCCURS & ALL PIPING IS IN ONE X,Z PLANE. FLOW IS 0.55 FT³/S @ 50 PSIG. WHAT RESULTANT FORCE BY WATER IS EXERTED ON EACH ELBOW.?

$$F_R = \sqrt{F_x^2 + F_y^2} = \left[\left[(PA(\cos\theta - 1)) + \frac{mv}{g_c}(\cos\theta - 1) \right]^2 + \left[(PA + \frac{mv}{g_c}) \sin\theta \right]^2 \right]^{1/2}$$

$$\left[(50 \text{ Psi}) \frac{144 \text{ in}^2}{\text{ft}^2} (0.049 \text{ ft}^2) (\cos 90^\circ - 1) + \frac{34.3 \text{ lbm}}{32.2 \text{ lbm ft/s}^2} (\cos 90^\circ - 1) \right]^2 + \left[(50 \text{ Psi}) \frac{144 \text{ in}^2}{\text{ft}^2} (0.049 \text{ ft}^2) \sin 90^\circ + \frac{34.3 \text{ lbm}}{32.2 \text{ lbm ft/s}^2} (11.2 \text{ ft/s}) \sin 90^\circ \right]^2$$

$A = \frac{\pi D^2}{4} = \frac{\pi (3)^2}{4} = 0.049$
 $v = \frac{Q}{A} = \frac{0.55}{0.049} = 11.2 \text{ ft/s}$

$$F_x = -381 \text{ lbf}$$

$$F_y = 381 \text{ lbf}$$

$$F_R = \left[(381)^2 + (-381)^2 \right]^{1/2} = 539 \text{ lbf}$$

5.9.1 Example Problem No. 1:

Refer to Figure 5-8-3, Page 5-28. $L_1 = 1000$ ft, $D_1 = 2$ ft,
 $e_1 = 0.005$ ft, $L_2 = 800$ ft, $D_2 = 3$ ft, $e_2 = 0.001$ ft, $v = 0.00001$ ft²/sec
 and $H = 20$ ft. What is the discharge Q through the system? ($K_e = 0.5$,
 $K_o = 1.0$)
entrance
outlet

Solution:

1. From the energy equation from A to B (including all losses)

$$H + 0 + 0 = K_{e_1} \frac{V_1^2}{2g} + f_1 \frac{L_1}{D_1} \frac{V_1^2}{2g} + \frac{(V_1 - V_2)^2}{2g} + f_2 \frac{L_2}{D_2} \frac{V_2^2}{2g} + K_{e_2} \frac{V_2^2}{2g}$$

hf in *hf pipe* *sudden Expansion* *hf pipe 2* *hf out*

2. From the continuity equation

$$V_1 D_1^2 = V_2 D_2^2$$

$$V_2 = \frac{V_1 D_1^2}{D_2^2}$$

3. $H = \frac{V_1^2}{2g} \left\{ K_e + \frac{f_1 L_1}{D_1} + \left[1 - \left(\frac{D_1}{D_2} \right)^2 \right]^2 + \frac{f_2 L_2}{D_2} \left(\frac{D_1}{D_2} \right)^4 + \left(\frac{D_1}{D_2} \right)^4 \right\}$

$$20 = \frac{V_1^2}{2g} \left\{ 0.5 + f_1 \left(\frac{1000}{2} \right) + \left[1 - \left(\frac{2}{3} \right)^2 \right]^2 + f_2 \left(\frac{800}{3} \right) \left(\frac{2}{3} \right)^4 + \left(\frac{2}{3} \right)^4 \right\}$$

After simplifying,

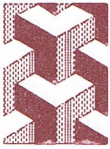
$$20 = \frac{V_1^2}{2g} (1.01 + 500 f_1 + 52.6 f_2)$$

4. The friction factors f_1 and f_2

$$\frac{e_1}{D} = 0.0025 \qquad \frac{e_2}{D} = 0.00033$$

From the Moody diagram, complete turbulence range choose *P-5-4*

$$f_1 = 0.025 \qquad f_2 = 0.015$$



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REVISIONS



SHEET NUMBER 1

JOB NAME: HYDRAULICS

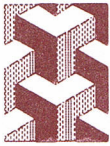
RE: _____

DATE 3/30/05

DETAILS

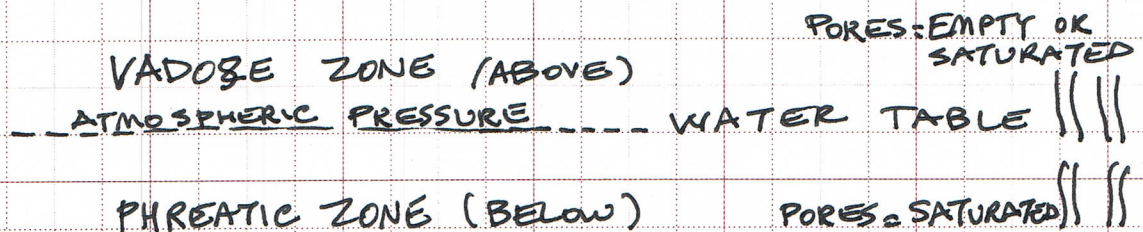
ENGINEERING & CONSULTING

A FARM MAINTAINS 500ha IN CURRENT PRODUCTION YEAR. SOD
REQUIRES 260CM OF WATER ANNUALLY. THIS IS APPLIED BY IRRIGATION
@ 2CM/hr THREE TIMES WEEKLY. LOT IS SUBDIVIDED EQUALLY.
WHAT IS THE MAXIMUM SUBDIVIDED PLOT SIZE IF IRRIGATION
AT SOD FARM IS TO OCCUR 12h/d & 7d/WK?



1. AQUIFERS

= SURFACE WATER = UNDERGROUND WATER =
SATURATED GEOLOGICAL FORMATION



RISE & FALL OF WATER TABLE = CHANGES IN VOLUME
(known as free Aquifer
or UNCONFINED AQUIFER)

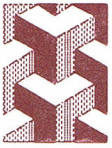
GRAVITY WELL = WATER LEVEL IN THE WELL CORRESPOND
TO WATER TABLE
"UNCONFINED WELL"

CONFINED AQUIFER = BOUNDED ON ALL EXTENTS
(MAY BE UNDER PRESSURE)

ONCE DRILLED, WATER IN THE WELL WILL RISE
TO A HEIGHT CORRESPONDING TO THE
HYDROSTATIC PRESSURE

PIEZOMETRIC HEIGHT OF RISE IS: $H = \frac{P}{\rho g} = \frac{P}{\gamma} = \frac{P}{\rho} \times \frac{\rho}{g}$

ARTESIAN WELL: IF CONFINED PRESSURE IS HIGH
ENOUGH, WATER WILL BE EXPELLED
FROM SURFACE



2. AQUIFER CHARACTERISTICS

SOIL MOISTURE CONTENT, w ; TENSIO METER, POROSITY,
VOID RATIO, EFFECTIVE POROSITY, HYDRAULIC GRADIENT

w , SOIL MOISTURE CONTENT (WATER CONTENT):

CHANGE IN MASS OF DRY SOIL & WET SOIL
CHANGE IN MASS AFTER OVEN DRYING OF SOIL

$$w = \frac{m_{\text{water}}}{m_{\text{soil}}} \quad \text{CAN BE DETERMINED BY TENSIO METER}$$

TENSIO METER: MEASURES VAPOR PRESSURE OF MOISTURE
IN THE SOIL

$$w = \frac{m_w}{m_s} = \frac{m_t - m_s}{m_s} \quad \text{t TOTAL}$$

POROSITY, n = PERCENTAGE OF VOID VOLUME TO TOTAL VOLUME
= $\frac{V_v}{V_t} = \frac{V_t - V_s}{V_t} = \frac{V_t - V_s}{V_v + V_s}$ also known as " θ "

WATER CONTENT = $\frac{\text{WEIGHT OF WATER}}{\text{WEIGHT OF SOIL}}$

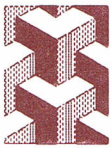
$$\text{VOID RATIO, } e = e = \frac{V_v}{V_s} = \frac{V_t - V_s}{V_s}$$

$$\text{VOID RATIO \& POROSITY} = e = \frac{n}{1-n}$$

EFFECTIVE POROSITY, n_e = 95 TO 98% OF TOTAL POROSITY
PORES ARE PLUGGED OR DEAD END

HYDRAULIC GRADIENT, i = $\frac{\text{CHANGE IN HYDRAULIC HEAD}}{\text{PARTICULAR DISTANCE}} = \frac{\Delta H}{L}$

HYDRAULIC HEAD: MEASURED PIEZOMETRIC HEAD AT
OBSERVATION WELLS



3. PERMEABILITY

OF LIQUID AFFECTED BY FLUID & MEDIUM
MEDIUM = INDEPENDENT OF FLUID PROPERTIES

INTRINSIC PERMEABILITY (SPECIFIC PERMEABILITY), k_s =
EFFECT OF MEDIUM

DARCY = UNIT of k , Length Squared = $0.987 \times 10^{-8} \text{ cm}^2$

Coefficient of PERMEABILITY = HYDRAULIC CONDUCTIVITY,
= PERMEABILITY, K
= DETERMINED BY TESTS
= $\frac{K \gamma}{\mu} = \frac{K \gamma}{\mu}$ length/sec
TIME

IN U.S. = MEINZER UNITS = $\frac{\text{GALLONS}}{\text{DAY ft}^2}$; NOW $\frac{\text{FE (m)}}{\text{DAY (DAY)}}$

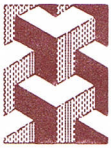
$K = C D_{\text{MEAN}}^2$
WHERE D^2 = SQUARE OF MEAN PARTICLE DIAMETER
PROPORTIONALITY CONSTANT

HAZEN'S EMPIRICAL FORMULA = APPROXIMATE COEF. OF PERM.
FOR CLEAN, UNIFORM SANDS.

$$K_{\text{cm/s}} \approx (D_{10, \text{mm}})^2 \quad [0.1 \text{ mm} \leq D_{10, \text{mm}} \leq 3.0 \text{ mm}]$$

- TESTS FOR K :
- (a) CONSTANT HEAD PERM. TEST (SAND)
 - (b) FALLING-HEAD PERM. TEST (FINE SAND & SILTS)
 - (c) CONSOLIDATION TEST (CLAY)
 - (d) FIELT TEST OF WELL (IN SITU GRAVEL & SANDS)

GRAVEL $K = 10^3 - 10^5 \rightarrow$ SANDSTONE $10 \rightarrow$ CLAY 10^{-3} DARCY'S
 $10^4 - 10^6 \rightarrow$ $10^2 \rightarrow 10^{-2}$ gal/day ft²



4. DARCY'S LAW

= MOVEMENT OF GROUND WATER THRU AN Aquifer, Re < 1

$$Q = -K i A_{gro} = -V_e A_{gro}$$

$$q = \text{SPECIFIC DISCHARGE} = \frac{Q}{A_{gro}} = K i = V_e$$

= EFFECTIVE VELOCITY = V_e

= ONLY $Re < 1$ (WHEN $Re = 2$, SIGNIFICANT CHANGES)

$$Re = \frac{\rho q D_{MEAN}}{\mu} = \frac{\rho D_{MEAN}}{\nu}$$

ρ	DENSITY	lbm / ft ³	Kg / m ³
μ	ABS. VISCOSITY	lb _f -sec / ft ²	Pa. S
γ	SP. WEIGHT	lb _f / ft ³	

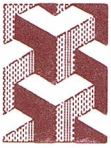
K	HYDRAULIC CONDUCTIVITY	ft ³ / DAY ft ²	m ³ / DAY m ²
-----	------------------------	---------------------------------------	-------------------------------------

q	SPECIFIC DISCHARGE	ft / s	m / s
-----	--------------------	--------	-------

Q	FLOW QUANTITY	ft ³ / s	m ³ / s
-----	---------------	---------------------	--------------------

i	HYDRAULIC GRADIENT	ft / ft	m / m
-----	--------------------	---------	-------

A	AREA	ft ²	m ²
-----	------	-----------------	----------------



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5. TRANSMISSIVITY

= COEFFICIENT OF TRANSMISSIVITY

= INDEX FOR RATE OF GROUNDWATER
MOVEMENT

Y

= SATURATED Aquifer THICKNESS

(ELEVATION: IMPERMEABLE BOTTOM - WATER TABLE)

b

= WIDTH

$$T = KY$$

$$\rightarrow K = \frac{T}{Y}$$

$$A_{gross} = Yb$$

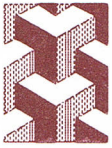
$$\rightarrow Y = \frac{A_{gross}}{b}$$

$$\Rightarrow K = \frac{Tb}{A_{gross}}$$

$$Q = -K_i A_{gross} = -Tb_i \frac{A_{gross}}{A_{gross}}$$

$$= |-Tb_i| = Tb_i$$

$$T = KY$$



26.14 FLOW NETS

GROUNDWATER MOVES FROM HYDRAULIC (HIGH) HEAD TO LOWER HEAD. RESULTING PATH OF FLOW IS CALLED "FLOW NET"

IDEAL CASE OF "GROUNDWATER SEEPAGE": STEADY, 2D, INCOMPRESSIBLE, HOMOGENEOUS MEDIUM, VISCOSITY IS CONSTANT

STREAMLINES (FLOW LINES) PATH OF SEEPAGE
EQUIPOTENTIAL LINES (CONTOURS) LINE OF CONSTANT H. HD
HYDRAULIC HEAD

FLOW NETS RULES

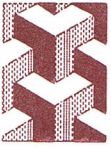
21.1 : STREAMLINES ENTER & LEAVE PREVIOUS SURFACES PERPENDICULAR TO THOSE SURFACES

21.2 : STREAMLINES APPROACH LINE OF SEEPAGE ASYMPTOTICALLY

21.3 : STREAMLINES ARE PARALLEL TO BUT CANNOT TOUCH IMPERVIOUS SURFACE

21.4 STREAMLINE IS IN DIRECTION FLOW

21.5 STEAM LINES ~ ARE FALL



DETAILS

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21-6 12. UNSTEADY flow

• NON-EQUILIBRIUM

• THESE EQUATION

$$S_{r,t} = \left(\frac{Q}{4\pi K Y} \right) W(u) \quad \rightarrow \text{WELL FUNCTION DIMENSIONLESS}$$

$$= \left(\frac{Q}{4\pi T} \right) W(u)$$

$$W(u) = -0.577219 - \ln u + u - \frac{u^2}{(2)(2)} + \left(\frac{u^3}{(3)(3!)} \right) - \frac{u^4}{(4)(4!)} + \dots$$

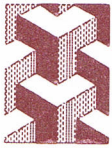
$$u = \frac{r^2 S}{4Tt}$$

$$S_1 - S_2 = y_2 - y_1 = \frac{Q}{4\pi K Y} (W(u_1) - W(u_2))$$

IF $u < 0.01$ use Jacob's

if $u_2 < 0.01$

$$\text{Jacob's eqn } S_{r,t} = \frac{Q}{4\pi T} \ln \left(\frac{4.53 T}{r^2 S} \right)$$



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FOR A 3mi² SQ. DRAINAGE BASIN A 2-HR RAINFALL DURATION OF 0.75 IN/HR UNIFORMLY OVER BASIN PRODUCES

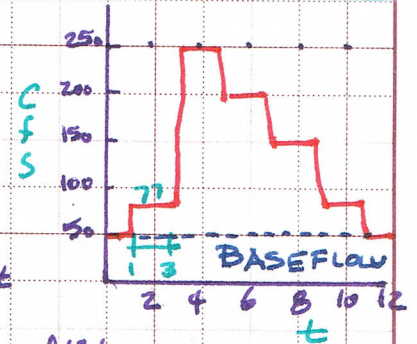
T-HRS	0	2	4	6	8	10	12
RUNOFF, CFS	50	77	250	200	150	70	50

FIND: 2-HR & 4HR HYDROGRAPH; TOTAL RUN OFF FROM A 1.5 IN/HR (4HR) DURATION
TOTAL RUN OFF 2.5 IN/HR, 1.2 IN/HR INFILTRATION 2 HR DURATION

TOTAL CFS (-BASEFLOW)

	0	2	4	6	8	10	12
	50	77	250	200	150	70	50
SUBTRACT	0	27	200	150	100	20	0
50							

$\sum \text{of } (0 + 27 + 200 + 150 + 100 + 20) * 2 \text{ HR} * \frac{3600 \text{ S}}{\text{HR}} * 1.2 \text{ IN/FT}$



$\sum \text{CFS RUN OFF} / (3 \text{ mi}^2 \text{ SQ} * 640 \text{ acre/mi}^2 * 43560 \text{ ft}^2/\text{acre})$

$P = \sum \text{RUN OFF} / \text{AREA} = 0.51 \text{ in}$

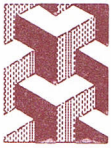
	0	2	4	6	8	10	12
	0	27/0.51	200/0.51	150/0.51	100/0.51	20/0.51	0
	0	53	392	294	196	39	0

UNIT HYDROPH

FOR 2-HR CONVERSION TO 4-HR

Int 2HR	0	53	392	294	196	39	0	0
		0	53	392	294	196	39	
SUM 4HR	0	53	445	686	490	235	39	0
4-HR (SUM/2)		26.5	222.5	343	245	117.5	19.5	4HR UHG.

INFILTRATION: RATE OF RAINFALL - RATE OF ACTUAL MEASURED RUNOFF
 $2 \text{ HR} * 0.75 \text{ in/HR} = 1.5 \text{ in in 2-HR} = (\text{NET RAINFALL} = 0.51) \leq 1.0 \text{ OR } 0.9 \text{ CFS}$

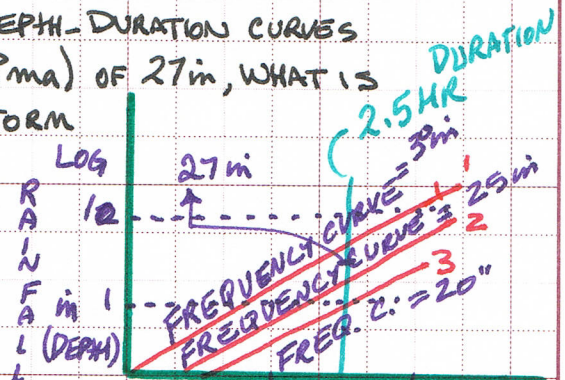
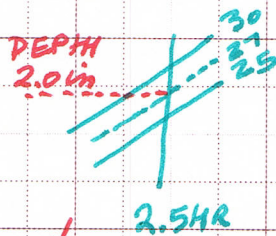


DETAILS

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25 YR RETURN PERIOD RAINFALL FREQUENCY-DEPTH-DURATION CURVES FOR A MEAN ANNUAL PRECIPITATION (P_{ma}) OF 27 in, WHAT IS RAINFALL INTENSITY FOR A 2.5 HR STORM

d = RAINFALL DEPTH, in
t = STORM DURATION, hr



$$I (\text{RAINFALL INTENSITY}) \text{ in/hr} = \frac{d}{t} = \frac{\text{RAINFALL DEPTH}}{\text{2.5 HR DURATION}} = \frac{2.0}{2.5} = 0.80 \text{ in/hr}$$

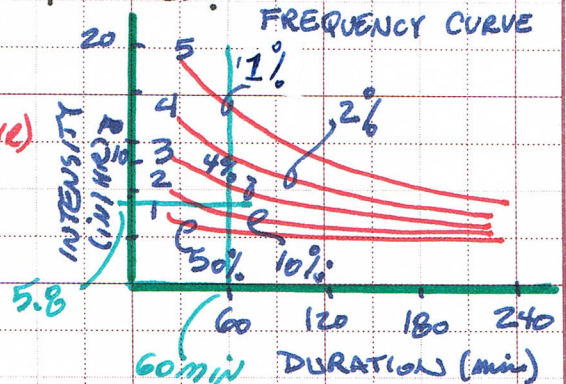
FREQUENCY-INTENSITY-DURATION CURVES SHOWN. WHAT IS FREQUENCY OF 60 MIN DURATION AND 5.8 in/hr INTENSITY STORM?

DURATION 60 MIN

INTENSITY (in/hr) = 5.8

CROSS SECTION OF 60 min & I = 5.8 (in/hr) GIVES CURVE # 4 OR 2%

2% means 2 TIMES EVERY YEAR OR ONE IN 50 YRS



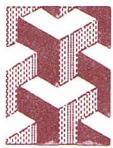
FACILITY WILL ACCEPT 1% RISK OF FLOODING DURING 50 YR. WHAT IS ANNUAL PROBABILITY THAT FLOODING WILL OCCUR DURING LIFE OF 50 YRS.

n PERIOD OF INTEREST = 50 YR

PF ANNUAL PROBABILITY OF FLOOD EVENT = $1 - (1 - R)^n$

R ACCEPTABLE RISK OF FLOOD EVENT = 1% = 0.01 OR 1/100

$$PF = 1 - (1 - R)^n = 1 - (1 - 0.01)^{50} = 0.00020 \text{ OR } 0.02\%$$



DETAILS

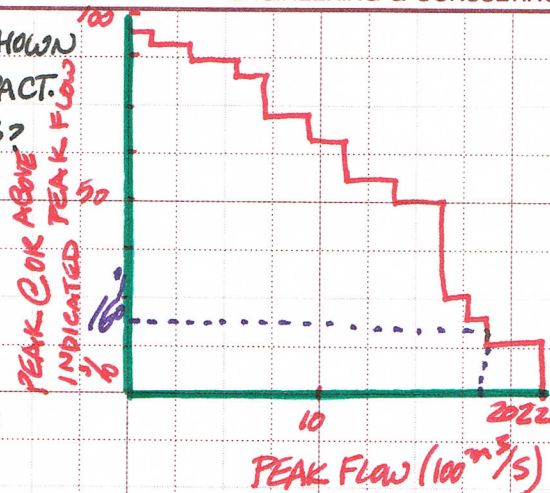
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HISTOGRAPH W/ 112 EVENTS OVER 94 YEARS SHOWN
IF LARGEST 18 EVENT CAUSED ECONOMIC IMPACT.
WHAT IS MINIMUM PEAK FLOW OF FLOODS?

I FLOOD CREATING ECONOMIC IMPACT %
 n_e NUMBER OF EVENTS
 n_f NUMBER OF FLOODS

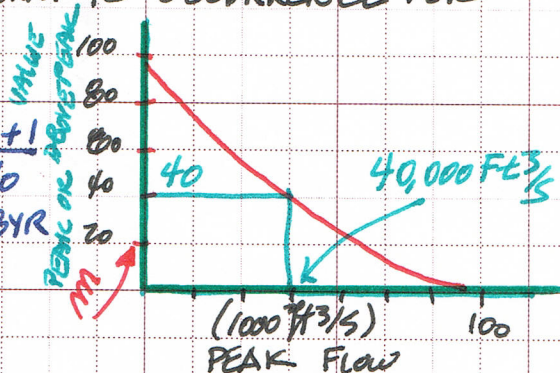
$$I = \frac{n_f (100\%)}{n_e} = \frac{\# \text{ OF FLOODS } 100}{\# \text{ OF EVENTS } 112} = \frac{18}{112} \times 100 = 16\%$$

OF PEAK FLOODS IN % @ 16% GIVES $\approx 1900 \text{ m}^3/\text{s}$ PEAK FLOW



HISTOGRAPH OF PEAK FLOW FOR 112 YEARS. WHAT IS OCCURRENCE FOR
EVENT FLOW OF $40,000 \text{ FT}^3/\text{s}$

T_p = RECURRENCE INTERVAL = $\frac{N+1}{m} = \frac{112+1}{40} = 2.8 \text{ YR}$
 N = PERIOD OF RECORD (112 YR)
 m = NO. OF EVENTS OF INTEREST THAT EXCEED THE PEAK FLOW



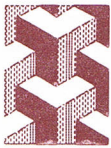
ANNUAL 97 YR FLOOD DATA: $\log \bar{X}$ (AVE. MEAN FLOOD FLOWS, FT^3/s) = 3.571;
SUM OF $[\log X (\text{EACH EVENT}) - \log \bar{X}]^2$; SUM OF $[\log X (\text{EACH EVENT}) - \log \bar{X}]^3$
WHAT IS MAGNITUDE OF 25 YEAR FLOOD?

USE "LOG PEARSON TYPE III" DISTRIBUTION TO FIND FLOOD MAGNITUDE
 N = # OF YEARS RECORD; X = FLOOD MAGNITUDE, FT^3/s , σ = STD DEVIATION

$$\sigma = \sqrt{\frac{\sum (X - \bar{X})^2}{N-1}} = \left[\frac{3.894}{97-1} \right]^{1/2} = 0.20; \text{ g Skew Coef} = \frac{N \sum (\log X - \log \bar{X})^3}{(N-1)(N-2) \sigma^3} = \frac{97(0.151)}{(96)(95)(0.2)^3} = 0.24$$

K: Log Pearson Type III Dist. Coef. w/ 25 YR & $g = 0.24 \rightarrow K = 1.833$ LOOK UP

$$\log x = \log \bar{X} + K\sigma = 3.571 + 1.833(0.2) = 3.938 \text{ (approx)} \rightarrow 8700 \text{ FT}^3/\text{s}$$

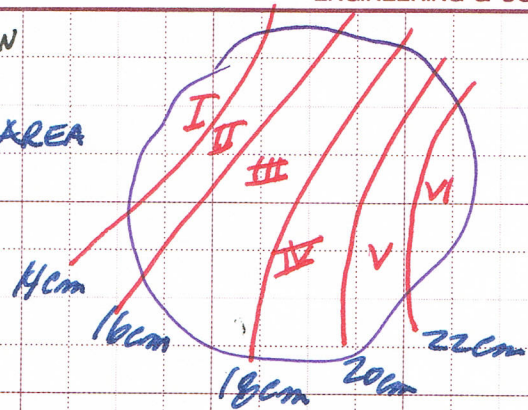


DETAILS

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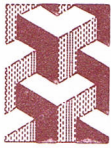
AN ISOMETAL MAP WITH AREA'S SHOWN
WHAT IS AVERAGE PERCIPITATION ?

AREA	ISOHYET Cm	CLOSED AREA Km ²
I	722	84
II	20	252
III	18	578
IV	16	892
V	14	1136
VI	<14	1294



BASED ON DATA

AREA	ENCLOSED ISOHYET	AREA Km ²	NET AREA	AVERAGE PERCIPITATION	PERCIPITATION VOLUME
I	722cm	84	84	* 23 =	1932 Cm Km ²
II	20	252	168	* 21	3528
III	18	578	326	* 19	6194
IV	16	892	314	* 17	5338
V	14	1136	244	* 15	3660
VI	<14	1294	158	* 13	2054
	A	B	C	D	E
			$C = B - B_{i-1}$	$D = A + 1$	$E = D * C$

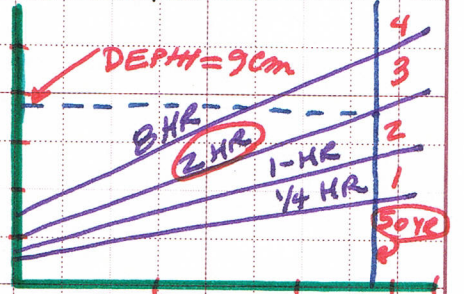


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GIVEN RAINFALL FREQUENCY-DEPTH-DURATION CURVE, STEEL FORMULA $K=80 \text{ IN-MIN/HR}$ & 25 MIN. (b). WHAT IS TIME OF CONCENTRATION FOR 2 HR 50YR STORM

STEEL FORMULA $L_i = \frac{K}{t_c + b}$
 INTENSITY \leftarrow L_i
 RAINFALL Depth cm
 DURATION hr
 $t_c + b$ 25 min
 TIME OF CONCENT. (min)
 depth (cm)

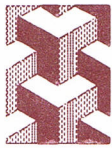


BASED ON 50YR RECURRENCE & CURVE 3 DURATION 2 HR (TE) } DEPTH = 9cm
 Recurrence 10 50 100 YR

$$L_i = \frac{d}{t} = \frac{9 \text{ cm Depth}}{2 \text{ HR DURATION}} = 4.5 \text{ cm/HR} = \frac{180 \text{ in-min/HR}}{2.91} = 1.8 \text{ in/HR}$$

INTERVAL (YR) LOG
 $t_c + 25$ $t_c = 75 \text{ min}$

$K = \text{UNIT} = \underline{\text{in-min/HR}}$ L_i MUST BE CONVERTED



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WITH 3200 POPULATION, WHAT IS MAXIMUM DAILY DEMAND DURING SUMMER INCLUDING FIRE DEMAND?

$$Q = Q_m P f_s f_p + Q_f = Q_m P f_s f_p + 1020 \sqrt{P} (1 - 0.01 \sqrt{P})$$

75 TO 130 POPULATION (SEASONAL) f SUMMER DAILY "PEAK" CORRECTION
INCREASED TO 160-165 ADDS 20-30% (OR 1.25) 50-100% OR (1.75) 75%
TAKE 165 G/PERSON-DAY (OR 1.25) 25% 75%

Q_f OR 500 GPM MIN

$$Q = \left(Q_m = \frac{165 \text{ G}}{\text{PERS-DAY}} \right) (1.25)(1.75)(3200) * \left(\frac{(1-\text{DAY})}{(1440 \text{ min})} \right) + 1020 \sqrt{3200} (1 - 0.01 \sqrt{3200})$$

$$= \frac{165 (1.25)(1.75) 3200}{1440} + 1792 = 2594 \text{ GPM}$$

(> 500 = OK)

BASED ON GIVEN DATA
WHAT IS PROJECTED APPROXIMATE
AVERAGE WATER DEMAND
IN 2002?

n : # of decades
 ΔP : POPULATION CHANGE FOR EACH DECADE
 ΔP_m : AVERAGE POPULATION CHANGE
 $\Delta P_m = \frac{\sum \Delta P}{n} = \frac{19,300}{8} = 2413 \text{ PEOPLE DECADE}$

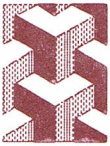
P_f (FUTURE POPULATION, 2020) =
(POPULATION @ 2000) 40,100 +
2 (DECADES) (2413 PERSON / DECADE)
40,100 + 2(2413) = 44,926 PEOPLE

ASSUME 140 GALLONS / DAY FOR NEXT 2 DECADE

$$Q_f = (140) \text{ GPD} * 44,926 \text{ PEOPLE} = 6.3 \times 10^6 \text{ GAL/DAY}$$

YEAR	POPULATION	PER CAPITAL WATER USE (G/DAY)
1920	20,800	83
1 1930	23,400	89
2 1940	25,100	94
3 1950	27,900	97
4 1960	29,800	137
5 1970	32,600	159
6 1980	35,200	148
7 1990	37,000	144
8 2000	40,100	142

Δ POPULATION PER 10 YRS
2600, 1700, 2800, 1900, 2800, 2600, 2500, 2400
TOTAL CHANGE 19,300



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AVERAGE WATER USE SHOWN. WATER IS PUMPED TO RESERVOIR AT CONSTANT RATE = AVE. DAILY DEMAND. DURING WHAT PERIOD OF DAY WILL THE NET WATER FLOW BE INTO RESERVOIR?

TIME	AVE. DEMAND GPM	
0 - 0200	6900	IN FILL
0200-0400	6500	IN "
0400-0600	8100	IN "
0600-0800	12100	OUT
0800-1000	14300	OUT
1000-1200	15,600	OUT
1200-1400	13800	OUT
1400-1600	12900	OUT
1600-1800	9900	FILL IN
1800-2000	8900	FILL IN
2000-2200	8300	FILL IN
2200-2400	7200	FILL IN

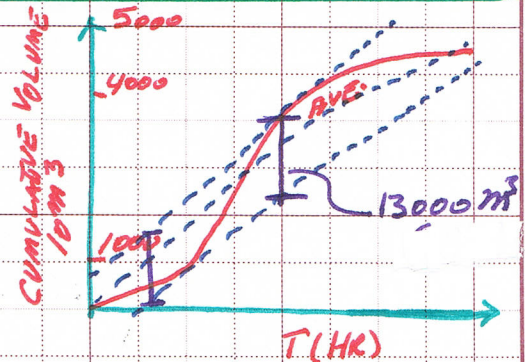
$Q_m = \sum q_m / n = 124,100 \text{ GPM} / 12 = 10,342$
 IF $Q_m >$ DEMAND FLOW IN (FILLING) RESERVOIR.

FROM 0600 TO 0800: FLOW 8100 → 12100 INTERPOLATE
 $0600 + (8:00 - 6:00) \frac{10,324 - 8100}{12,100 - 8,100} = 0600 + 1.1 \text{ hr}$
 $= 7:10 \text{ a.m.}$
 $1800 - (1600 - 1800) \frac{10,324 - 9900}{12,500 - 9900} = 1800 - 0.33 \text{ hr}$
 $= 1740 (5:40 \text{ PM})$
 $\sum q_m = 124,100$

MASS DIAGRAM: FOR A MUNICIPAL WATER TANK. WHAT IS MINIMUM REQUIRED CAPACITY OF STORAGE TANK?

- DRAW AVE LINE. FROM 0 TO MAX. @ 24 HRS
- DRAW PARALLEL TO TANGENT (LOW & HIGH)
- VERTICAL DIFFERENCE IS MIN TANK REQ.

$13,000 \text{ m}^3$

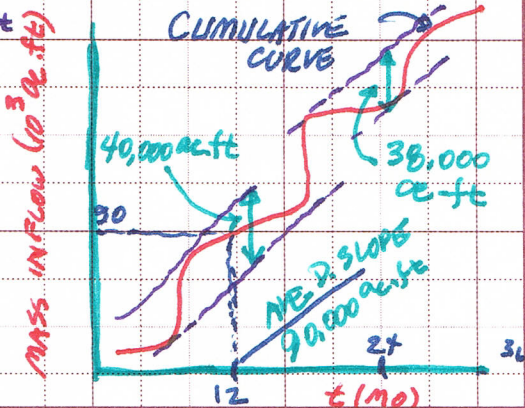


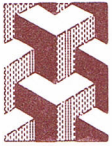
RESERVOIR (IRRIGATION WATER). REQUIRED MIN. ANNUAL YIELD = 90,000 ac-ft. INPUT TO RESERVOIR: SEVERAL SMALL STREAMS. MASS INFLOW FOR 3 YR SHOWN. WHAT RESERVOIR CAPACITY REQUIRED TO MEET MIN YIELD?

- ONCE CUMULATIVE RESERVOIR REACHES TO 90,000 ac-ft @ 12 MONTHS.

- PARALLEL TO CURVE GIVE MIN & MAX POINT

VOLUME OF CAPACITY: SLOPE LOWER OR HIGHER Δ IN PARALLEL WORK 40,000 ac-ft





CALCULATE POWER FOR WATER SUPPLY & REQUIRED STORAGE.

METHODS FOR SAFE YIELD OF WATERSHED FROM STORAGE:

(a) MASS CURVE OF MODIFIED RUNOFF

USE RECORD (MONTHLY) FROM STREAM GAGING STATION.

IDENTIFY DROUGHT PERIODS

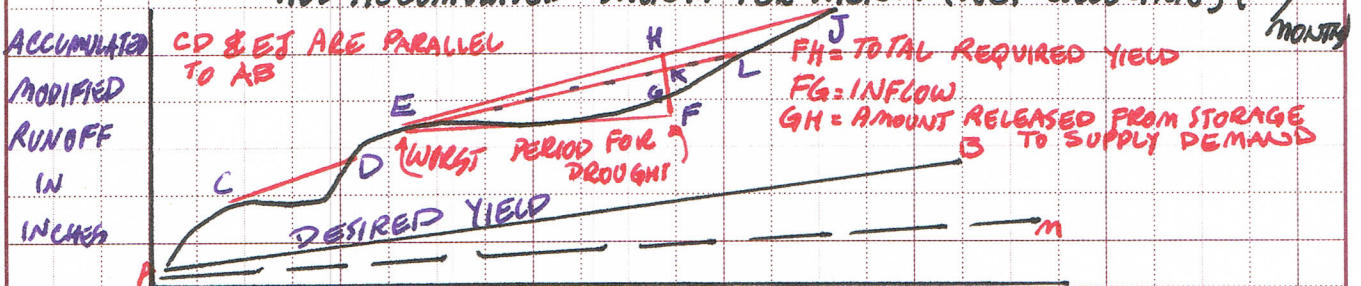
IF IN CFS CONVERT TO DEPTH OF STREAM

ACCOUNT FOR EVAPORATION LOSS

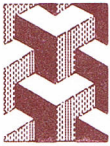
ACCOUNT FOR CUSTOMER / OWNER USE (PERIODIC)

ACCOUNT FOR FULL STORAGE / WASTE ON SPILLWAY

ADD ACCUMULATED MONTH PER MONTH (NET COLLECTION) (in/month)



IF "AB" IS DESIRED YIELD & EJ (PARALLEL)
STORAGE IS NOT ECONOMICAL EKL OR GK STORAGE MAY BE SUITABLE.
THEN EKL PARALLEL BECOMES "AM" NEW YIELD DESIRED.



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40,000 PERSON COMMUNITY

MAX. DAILY CONSUMPTION = $200 \times 40,000 = 8 \text{ MG}$

1ST PARALLEL TO MAX. TANGENT Y. DROP VERT. RUN

2ND " " MIN TANGENT X

b-b' LIMITS OF RESERVOIR CAPACITY

$$175 - 90 = 85 \text{ GPCD} \times 40,000 = 3.4 \text{ MG}$$

FOR FIRE FLOW NEEDED Q, $Q = 1020\sqrt{P}(1 - 0.01\sqrt{P})$
 $= 1020\sqrt{40}(1 - 0.01\sqrt{40}) = 6054 \text{ GPM}$

RECOMMEND 10-HRS FOR TOWNS > 2500 POPULATION

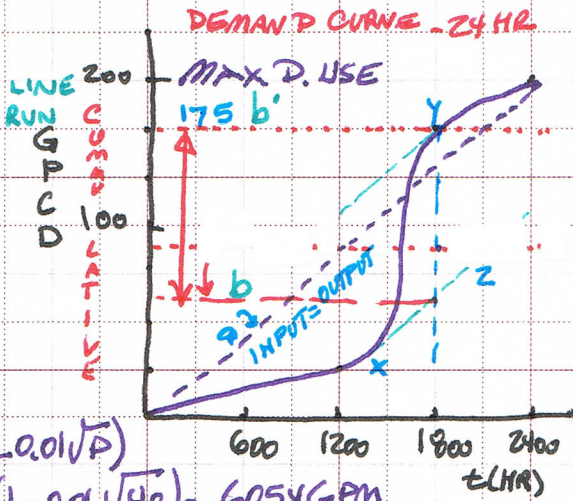
$$(6045) 60 (10) = 3.63 \text{ MG}$$

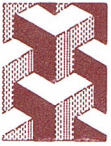
$$\text{GENERAL DEMAND} + \text{NFF} = 3.63 + 3.4 = 7.03 \text{ MG}$$

NORMAL PUMP WORKS FOR $8 \text{ MG} / 24 \text{ HRS} = 0.33 \text{ MG/HR}$. IF 16-HR PUMP
 RATE IS $8 \text{ MG} / 16 = 0.5 \text{ MG/HR}$.

$$\text{THE } 7.03 \text{ MG} \times 24 \text{ HRS REQUIRED} / 16 \text{ MG OPERATION} = \underline{\underline{10.55 \text{ MG/HR}}}$$

16 HRS





DETAILS

ENGINEERING & CONSULTING

PRESSURE REQUIRED: 20 TO 40 PSI; MINIMUM WITH TRUCK PUMPER
40 TO 75 PSI DIRECTLY FROM HYDRANTS
60 TO 80 PSI; STATIC PRESSURE
100 PSI OR LARGER, STORAGE @ ELEVATIONS

REQUIRED FLOW $Q_{DESIGN} = Q_{HOURLY} (MAXIMUM)$

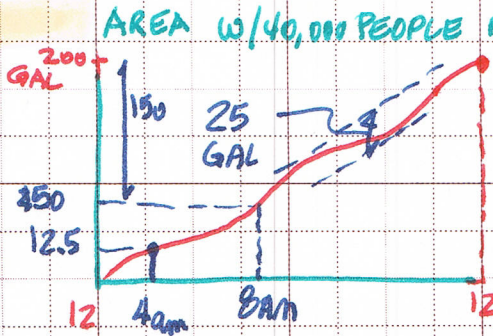
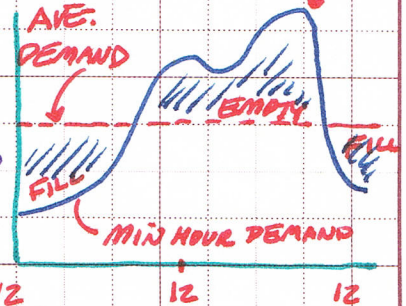
$= Q_{DAILY} + Q_{FIRE}$
(MAX. PAST 3 YRS, DAILY FLOW)

$Q_{FIRE} = f(AREA, CONSTRUCTION, HEIGHT, LOCAL CODES, FIRE HAZARD)$

$Q_{FIRE} = 18 C A^{0.5}$ $C = 1.5$ COMBUSTIBLE MAT'L
0.6 **MAX. HR DEMAND**

ADD 10% FOR LOSSES

STORAGE: $\approx 30\%$ OF TOTAL DAILY USE
FIRE FLOW STORAGE 1 → 6 HRS



PER CAPITA PER DAY = 200 GAL

$25 \text{ GAL} \times 40,000 = 1 \times 10^6 \text{ GAL STORAGE}$
TANGENT TO LINES

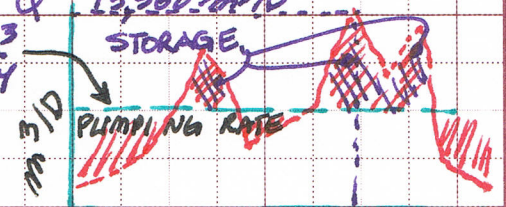
WHILE PUMP IS ON 4:00am to 8:00am & STORE FOR OTHER TIME. STORES NEEDED

$(12.5 + 150) 40,000 = 6.5 \times 10^6 \text{ GAL STORAGE}$

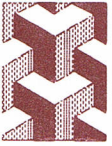
24 HR DISTRIBUTION. PUMP @ $3.6 \text{ m}^3/\text{min}$ CONTINUOUS. ADD STORAGE.

WHAT IS MAX. PUMPING IF NO STORAGE? STORAGE W/ 24HR @ $3.6 \text{ m}^3/\text{min}$?

- MAX. Q REQUIRED $13,500 \text{ m}^3/\text{D}$ $Q = 13,500 \text{ m}^3/\text{D}$
- @ $3.6 \text{ m}^3/\text{min} \times 24 \text{ HRS} \times 60 \frac{\text{min}}{\text{HR}} = 5184 \frac{\text{m}^3}{\text{DAY}}$
- STORAGE: AREA ABOVE AVE. PUMP CURVE.



$30 \text{ SQUARE} (1\text{-HR} \times 1000 \frac{\text{m}^3}{\text{DAY}}) \frac{1 \text{ DAY}}{24 \text{ HR}} = 1,250 \text{ m}^3$



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SHEET NUMBER _____

JOB NAME: ENVIRONMENTAL

RE: STORAGE

DATE 5-15-05

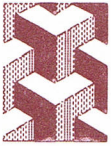
DETAILS

ENGINEERING & CONSULTING

STORAGE

RESERVOIR OR WATERTANK/TOWERS TO ACCOUNT FOR DAILY /
SEASONAL WATER DEMAND AS WELL AS DEMAND FOR FIRE FIGHTING
STORAGE ALLOWS DESIGN CAPACITY TO BE LESS THAN PEAK
WATER DEMAND

- COPPER SULFATE IS USED IN SHALLOW PORTIONS OF RESERVOIRS FOR ALGAE



DETAILS

ENGINEERING & CONSULTING

346 SINGLE FAMILY HOMES (1/2 ac each). EQUALLY DIVIDED ONE & TWO STORY WOOD FRAME, 1400 FT² & 2300 FT², RESPECTIVELY. AVERAGE NO. OF PERSONS IS 4 PER FAMILY. MOST NEARLY WHAT DESIGN FLOW SHOULD THE WATER LINE SERVICING THE DEVELOPMENT?

$$Q_d = Q_{FA} \text{ (FIRE DEMAND)} + Q_P \text{ (PEAK DAILY DOMESTIC)}$$

(1) IF DISTANCE BETWEEN HOUSES 30' → 100'
 Q_{fd} (BASED ON DISTANCE-TABLE) = 750 GPM

(2) BASED ON WORST CASE
 2 STORY UNIT
 A AREA FT²
 F DWELLING FACTOR
 1.5 WOOD FRAME

$$(346 \text{ HOUSE}) \left(\frac{4 \text{ PEOPLE}}{\text{HOUSE}} \right) = 1384 \text{ PEOPLE}$$

$$\left(\frac{165 \text{ GAL}}{\text{PERSON-DAY}} \right) \left(\frac{1\text{-DAY}}{1440 \text{ MIN}} \right) = q$$

$$Q_{FA} = 18F \sqrt{A} =$$

$$= 18(1.5) \sqrt{2300} =$$

$$= 1295 \text{ GPM}$$

NEAREST TO 250 GPM
 $\approx 1250 \text{ GPM}$

$$Q_a = (1384 \text{ PEOPLE}) \left(\frac{165 \text{ GAL}}{\text{PERSON-DAY}} \right) \left(\frac{1 \text{ DAY}}{1440 \text{ MIN}} \right)$$

$$= 159 \text{ GAL / MIN}$$

$$Q_P = (159 \text{ GPM}) \cdot 1.5 = 238 \text{ GPM}$$

PEAK DAILY FLOW MULTIPLIER = 1.5

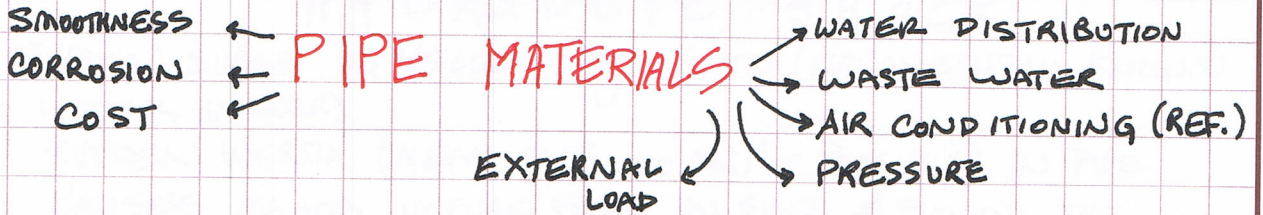
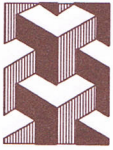
(3) BASED ON POPULATION
 $Q_{FP} = 1020 \sqrt{\frac{P}{1000}}$
 $(1 - 0.01 \sqrt{\frac{P}{1000}})$
 $= 1020 \sqrt{1384}$
 $(1 - 0.01 \sqrt{1384})$
 $= 1186 \text{ GPM}$
 $1250 > 1186 > 750 \therefore 1250 \text{ GPM}$

$$Q_d = Q_{FA} + Q_P$$

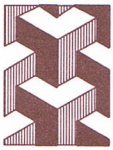
$$= 1250 + 238$$

$$= 1488 \text{ GPM}$$

$$\approx 1500 \text{ GPM}$$



MATERIAL	DESCRIPTION
• DUCTILE CAST IRON	STRONG, COSTLY, HEAVY, IMPERVIOUS, SCOUR RESISTANCE
• GRAY CAST IRON	SAME AS DUCTILE CAST IRON
• ASBESTOS CEMENT	LIGHT WEIGHT, CORROSION RESISTANCE, NO ELECTROLYSIS, WEAK STRUCTURALLY
• CONCRETE	WATER TIGHT, DURABLE, SMOOTH INTERIOR, LOW ^{MAINTENANCE}
• VITRIFIED CLAY	CORROSION RESISTANCE, SCOUR, EROSION, RESISTANCE
• STEEL	DUCTILE, HIGH STRENGTH, SMOOTH INTERIOR, SUBJECT TO CORROSION, RESISTANCE TO SHOCK
• PLASTIC	PVC & ABS; CHEMICALLY INERT, CORROSION RESISTANCE LOW COST
• COPPER & BRASS	WATER, CONDENSATE, ...



HYDRAULIC SHOCK SIMPLIFIED EQUATION PRESSURE INCREASE →
$$P (\text{PSI}) = 0.070 L (\text{FT PIPE RUN}) \text{ VELOCITY FPS} / t \text{ VALVE CLOSURE TIME (S)}$$
$$= 0.070 L V / t$$

AIR CHAMBERS: S HOCK ABSORBERS, A PIECE OF SAME DIAMETER PIPE (12" TO 24") CAN BE USED AS WELL. OVER YEARS AIR CHAMBERS SHOWN FAILURE & USELESS. THEY MUST BE CORRECTLY SIZED (VOLUME OF AIR), SIZE AIR CHAMBERS, PERIOD OF PRESSURE, ... REQUIRED FOR SIZING. INERT GAS/AIR CHAMBER WITHIN MEMBRANES WORK & ONCE SEALED AIR PRESSURE IS STABLE & DO NOT LEAK. EFFECTIVE OPERATION.

SWING VALVE IN DISCHARGE SIDE OF PUMPS: DURING PUMP SHUT DOWN, WATER REVERSAL CAUSE SLAM OF GATE CAUSING SHOCK WAVES.

SPRING VALVES TO BE USED & DESIGNED TO CLOSE EXACT MOMENT WATER FLOW CHANGES
NO CHANGE IN FLUID VELOCITY, THEREFORE: NO HYDRAULIC SHOCK WAVES



PIPE DAMAGES

OTHER THAN HYDRAULIC SHOCK,
EROSION, NOISE, & CAVITATION ARE OTHER ISSUES.

CAVITATION: SPONTANEOUS VAPORIZATION OF FLUID IS BASED ON WHEN PRESSURE OF FLUID IS THE LESS THAN VAPOR PRESSURE OF THAT FLUID (WITHIN THERMODYNAMICS OF FLUID). POCKETS OF VAPOR CREATED IS CALLED CAVITY THIS CAN OCCUR WITHIN PUMPS OR SOMETIMES UPSTREAM OF SUCTION SIDE OF PUMP, AS VAPOR CAVITY APPROACHES IMPELLER, NOISE, VIBRATION, IMPELLER PITTING, & STRUCTURAL DAMAGE OCCUR.

WITHIN PIPES, WHEN DIRECTION OF FLOW CHANGES SHARPLY & VELOCITY IS HIGH, CAVITATION OCCURS. SHORT RADUIS PIPES @ HIGH VELOCITY, CAUSES MAJOR CHANGE IN PRESSURE WITHIN FLUID, THUS CAUSING CAVITY. BUBBLES COLLAPSE DOWNSTREAM WITHIN PIPES.

NOISE: PART OF HYDRAULIC SHOCK, CAVITATION CAN BE REDUCED BY LOWERING VELOCITY WITHIN PIPES

EROSION: PIPES DEPENDING ON MATERIAL, FLUID, SOLID CONTENT, TEMPERATURE, VELOCITY HAVE DIFFERENT EROSION ISSUES. PIPE ELBOWS, CONNECTIONS, SURFACE ROUGHNESS, CALCIUM BUILDUPS, ARE ALL FACTORS OF ABRASION PROCESS & EROSION. HPS & BPS ARE NOW LIMITS OF HOT & COLD PIPE WATER VELOCITIES BY CODE.



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DATE: _____ SHEET: _____

PROJECT: _____

SUBJECT: _____

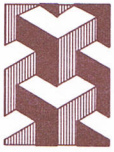
RE: _____

DETAILS

CIVIL . STRUCTURAL . ELECTRICAL . MECHANICAL . PLUMBING . ENERGY . LEED . GREEN

ENGINEERING & CONSULTING

HYDROMETER



- SCOPE** **BUDGET** **CODES** **SBCUSWGⁿ** **PROJECT INITIAL TASKS** **UTILITIES** **SEWER** **WATER** **GAS**
- SCOPE OF WORK:
VARIES FOR ALL PROJECTS & "SCOPE CREEP" MAY BECOME MAJOR CONCERNS THROUGHOUT WORK
 - IDENTIFY & TRANSCRIBE CLEAR/STERWISE SCOPE OF WORK & VERIFY WITH ALL FOR ITS ACCURACIES.
 - LIST & IDENTIFY ALL PLAYERS IN PROJECT
 - NOTIFY PARTIES (P.M., ETC.) ALL WORK BEYOND SCOPE OF WORK
 - CONSTRUCTION BUDGET
IDENTIFY THE TYPE OF BUILDING & PROVIDE \$/SQFT OR COMPLETE CONSTRUCTION COST. ESTIMATING BOOKS MUST BE CURRENT & MATCH LOCALITIES (R.S. MEANS, ETC.)
BUDGET CONTROLS DESIGN
 - A.H.J. (AUTHORITIES HAVING JURISDICTIONS), CODES, LAWS, & GUIDELINES.
FULL IDENTIFICATION OF ALL APPLICABLE LAWS IS CRITICAL. INDIVIDUALS ADMINISTERING ARE IMPORTANT: PLAN CHECKERS, INSPECTORS (PLUMBING, MECHANICAL, FIRE, HEALTH, WATER, SEWER, INSURANCE CO., BUILDING, ...)
THERE ARE MANY NATIONAL CODES IPC, UPC, APA, OSHA, IBC, AND MANY LOCAL CODES & AMENDMENTS.
 - UTILITIES: INVESTIGATE LOCAL CONDITIONS, CREATE UTILITY SITE PLANS
WATER, SANITARY, STORM, GAS, ELECTRIC, TOPOGRAPHY (CONTOUR LINES), RIGHT-OF-WAY'S (EASEMENTS), HARDSCAPE VS LANDSCAPES, CAPACITIES, SIZES, PRESSURES, MATERIALS. THIS MUST BE COORDINATED WITH CIVIL ENGINEER (IF AVAILABLE), ELECTRICAL & ALL UTILITY COMPANIES, PUBLIC WORKS, OR ANY OTHER AGENCIES. BACKFLOW DEVICES MAY APPLY.
 - SEWER: ALL OF #4 CONDITIONS APPLY. POINT OF CONNECTION, ELEVATION, SLOPES, LATERALS, MANHOLES, (INVERT, & TOP OF ELEVATIONS), LOADING CAPACITIES, POSSIBLE SURCHARGE ISSUES. THE LATERAL CONNECTIONS TO BUILDINGS,
 - WATER: ALL OF #4 CONDITIONS APPLY. METER, VALVES, BACK FLOW DEVICES, PRESSURE CAPACITIES FOR FIRE, DOMESTIC USE,
 - GAS: ALL OF #4 CONDITIONS APPLY. METER, VALVE, PRESSURE, BTU CONTENT, P₉₀, MATERIAL, ...



CLEANOUTS: CLEANOUTS PIPES MATCH PIPE SIZE UP TO 4" (6", 8", ...) 4" O.K.

- ANY CHANGE IN DIRECTIONS $> 45^\circ$
 - INSIDE/OUTSIDE BUILDING @ POINT OF EXIT (WYE BRANCH OR HOUSE)
 - 50 FT MAX. DISTANCE 4" OR LESS, 100 FT FOR LARGER $> 4"$ (TRAP)
 $> 10"$ REQUIRES MANHOLE @ EVERY DIRECTION CHANGE OR 150 FT.
 - BASE OF ALL STACKS.
- PROPER ACCESS (18-24" CLEAR), FOR ROTTO RODDERS, FIXTURE REMOVAL AS ACCORDS TO CLEANOUT ACCEPTABLE.

WASTE:

INDIRECT WASTE: INDIRECT CONNECTION TO SANITARY TRAPPED, VENTED. & DISCHARGE OULET SHOULD BE 1.5 TIMES INDIRECT PIPE SIZE ABOVE FLOOD LEVEL. CLEAN OUTS MANDATORY SINCE MANY BLOCKAGE BECAUSE OF LOW VELOCITY & LOW FLOW.

INDIRECT WASTES: SINKS, LAVATORIES, CONDENSATE DRAIN S. EXTREME PNEUMATIC EFFECTS DUE TO LOW RATE OF FLOW

SPECIAL WASTES

- TANK OVER FLOW, TANK EMPTYING LINES, RELIEF VALVE DISCHARGE SHOULD BE INDIRECT WASTE DUE TO OVER PRESSURIZATION
- DISCHARGES WITH AIR BREAK (F.S., ROOF DRAIN, ...)
- SAME FOR COOLING JACKETS, DRIP TRAYS PANS, STEAM EXPANSION BOILER OVERFLOWS, ...

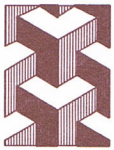
RATE OF FLOW IN FIXTURES

RATE OF FLOW, RATE OF DRAINAGE

$V = Q = 13.17 d^2 h^{1/2}$
 $\frac{gpm}{in^2} = \frac{ft}{ft}$

IN BRANCHES

- BRANCHES = Σ FLOW FIXTURES TO BRANCH
- UNIFORM FLOW
- BRANCH EXTENDED $> 5'$ DEV. LENGTH
- HYDROSTATIC PRESSURE = SURCHARGING
- IN SHORT RUNS, DUE TO HIGH VELOCITY SURCHARGE & COWS
- BRANCH Q OR $V <$ STACK V , Q OR YOUNG Q , V
- Q INTO STACK CANNOT DISTURB STACK
- OR BACK PRESSURE INTO BRANCH
- STACK FLOW MAX = $\Sigma Q_{STACK} + Q_{BRANCH}$



SCOURING: TO INSURE SAND, GRIT, PEBBLES, & OTHER SOLIDS ARE IN SUSPENSION, THE FLUID FLOW MUST BE AT MINIMUM TERMINAL VELOCITY. THIS WILL INSURE NO WASTE DEPOSITION & BLOCKAGE. 2 FPS IS MINIMUM & 4 FPS MINIMUM FOR GREASY CONTENT FLUID FOR 2" & 1 1/2" PIPE WITH FULL OR 1/2 FULL FLOW FLOW VELOCITIES IN DRAINAGE PIPING ARE 1.98 & 1.85 FPS (LESS THAN 2 FPS). MINIMIZE LENGTHS OF 1 1/2" & 2" PIPE.

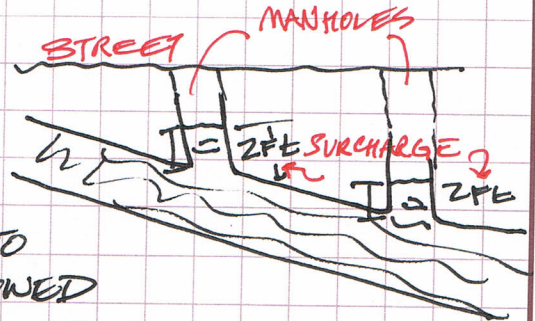
SURCHARGING

TO ACCOMMODATE OVERFLOW OR CERTAIN PEAK LOADS, OR WHEN SEWER & STORM DRAINAGE ARE COMBINED, SURCHARGING IS POSSIBLE EVENT & MUST BE ACCOUNTED FOR.

VERTICAL DISTANCE WITHIN MANHOLE IS MEASURE OF SURCHARGING.

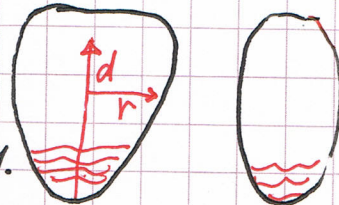
THIS MEASURE IS THE LEVEL ABOVE GRAVITY "FULL FLOW" CONDITIONS.

OPTIONS: SMALLER PIPE USED FOR NORMAL CONDITIONS & LESS SLOPE TO MEET TOPOGRAPHY. SURCHARGE IS ALLOWED OVER CAPACITY FOR ABNORMAL CONDITIONS.



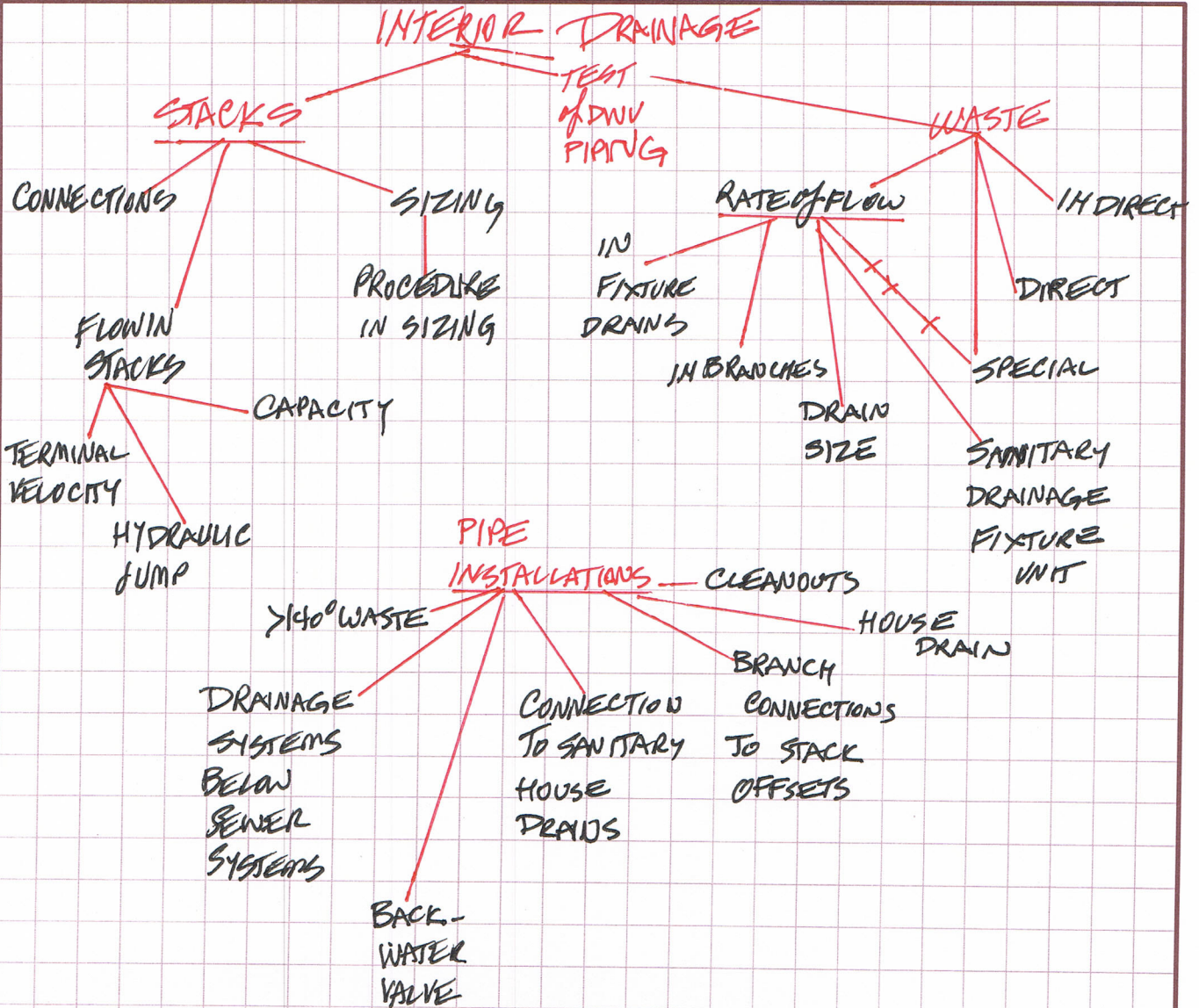
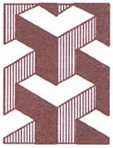
SEWER SHAPES.

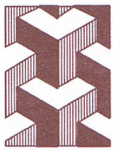
VARIABLE PIPE SHAPES WILL ALLOW HIGHER TERMINAL VELOCITY IN LOW FLOW CONDITIONS & @ HIGHER FLOW RATES, THE VELOCITY COULD REMAIN THE SAME $V = Q/A$ AS Q INCREASES, A INCREASES HYDRAULIC RADIUS INCREASES



SANITARY SEWER: PUBLIC (WHEN AVAILABLE) & PRIVATE. IN ALL CASES FULLY CONTAINED & NEVER @ HUMAN REACH. NEVER MIX WITH STORM WATER UNLESS FULLY TREATED

COMBINED SEWER & STORM SYSTEM: NOW EXTREMELY RARE, ALL COMBINED NOW MUST BE TREATED BEFORE REUSE OR DISCHARGE, STORM SOMETIMES USED AS OVERLOAD INTO SEWER SYSTEMS.





STACKS VERTICAL SEWER PIPING
COLLECTS HORIZONTAL BRANCHES

"SOIL" STACK: FECAL MATTER (WATER CLOSET) & URINALS

"WASTE" STACK: SHOWER, SINKS, LAVATORIES

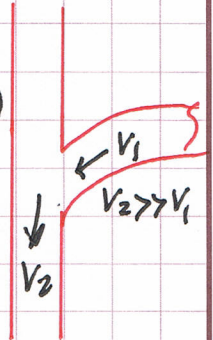
CONNECTIONS: HORIZONTAL TO VERTICAL (SANITARY TEE)

VERY HIGH VELOCITIES CREATE SELF SIPHONIC OF TRAPS.

TEE-WYE: "SAME" AS: COMBINATION WYE & "ONE EIGHTH WYE"

SANITARY TEE: ONLY IN VERTICAL POSITION

TEE WYE: IN ANY POSITION



FLOW IN STACKS. FEARS ARE: HIGH VELOCITY CAUSING UNWANTED IMPACT FLOW, SLUG OR FULL FLOW CAUSING SIPHONAGE & SUCTION OF WATER IN TRAPS, CREATION OF PRESSURE FLUCTUATIONS DUE TO PLUG FLOW (MAX ± 1" H₂O)

TERMINAL VELOCITY

GRAVITATIONAL FLOW WILL REACH EQUILIBRIUM

WITH WALL FRICTIONAL FORCES (ASSUMING

NO ADDITIONAL FLOW IS ADDED), @ THIS STAGE

VELOCITY REMAINS RELATIVELY CONSTANT

OR "ULTIMATE" VELOCITY OR TERMINAL

VELOCITY. WHICH IS ACHIEVED @ "TERMINAL

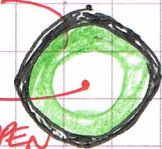
LENGTH" $V_T \approx 10 \rightarrow 15$ FPS WITHIN $L_T \approx 10 \rightarrow 15$ FEET

THEREFORE V_T IS IRRESPECTIVE OF L_T

& WITHIN 3 STORY SAME BEHAVIOR AS 50 STORY

SHEET OF WATER
1/4 TO 1/3 OF PIPE
AREA

CORE 3/4 OR 2/3 OPEN



$$V_T (\text{TERMINAL}) = 3 \left(\frac{V}{d} \right)^{2/5}$$

$$L_T (\text{TERMINAL}) = 0.052 V_T^2$$

$$V = Q = \text{FLOW RATE}$$

$$d = D = \text{STACK DIAMETER}$$

CAPACITY OF STACKS

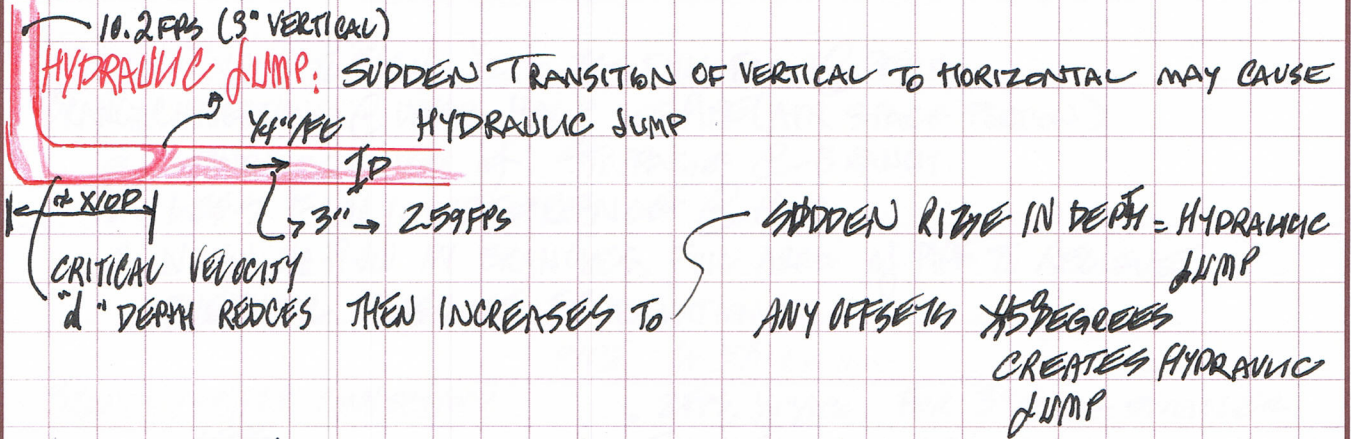
PLUG / SLUG FLOW DOES NOT OCCUR TILL $A_f = \left(\frac{r}{3} \text{ of } A_{\text{TOTAL}} \right)^{1/4}$

$$Q_{\text{MAX}} = V_{\text{MAX}} = 27.8 V^{2/3} d^{1/3}$$

PIPE	2	3	4	6	8	10
MAXIMUM CAPACITY OF STACKS (GPM)	($r^{1/4}$) 18.5	$r^{7/24}$ 54	70	($r^{1/3}$) -	85	95
		112	145	180	215	255
		330	435	530	635	740
		770	920	1145	1395	1645
		1300	1650	2065	2535	3005

$V = \frac{\text{AREA OF FLOW}}{\text{AREA OF PIPE}}$

UPPER LIMITS DIAPHRAGMING



DISTANCE OF OCCURANCE OF HYDRAULIC JUMP =

f(ENTRANCE VELOCITY, DEPTH OF HORIZONTAL WATER,
PIPE ROUGHNESS, PIPE DIAMETER, SLOPE)

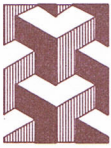
JUMP REDUCES WHEN PIPE DIAMETER, SLOPE, & PIPE INCREASE
SURGING DIES WITH PIPE ROUGHNESS

HIGH TEMPERATURE WASTE: HIGH TEMPERATURE CAUSES PIPE EXPANSION
EXCESSIVE CONTRACTION & EXPANSION WILL DAMAGE PIPES.

BOILERS, RESTAURANT DRAINS MUST BE COOLED BELOW 140°F
BEFORE DISCHARGING. THIS CAN BE DONE AS ENERGY CONSERVA-
TION TECHNIQUE AS WELL.

DRAINAGE BELOW SEWER LINES: VERIFY ALL OPTIONS BEFORE
DESIGNING UNDER SUCH CONDITIONS. EJECTOR/PUMPS ARE REQUIRED
(TIGHT & VENTED) CONDITIONS.

BACKWATER VALVE: SEWER BACKWATER VALVES OCCUR WHEN
STREET SEWER SYSTEM IS CLOGGED & BUILDING IS FLOODED
WITH PUBLIC SEWAGE. ONE BACKWATER VALVE TO SERVE UNITS
LOWER THAN SEWER PIPE IS REQUIRED. OTHER FLOORS NOT EFFECTED
WILL BE SEGREGATED WITH INDEPENDENT MAIN SEWER CONNECTIONS.



DOMESTIC WATER

SUBJECT IS USED IN PLUMBING, MECHANICAL, CIVIL, & CHEMICAL ENGINEERING. $Re > 4000$ - TURBULENT, $Re < 2300$ LAMINAR FLOW OCCURS WHEN MEASURING OR CALCULATING $Re = \frac{DVP}{\mu}$

TURBULENT FLOW OCCURS $\frac{1}{2}$ " , 1" , 2" PIPES

$V > 0.676$, 0.338, 0.169 FPS @ 50°F

$V > 0.247$, 0.124, 0.0617 FPS @ 140°F

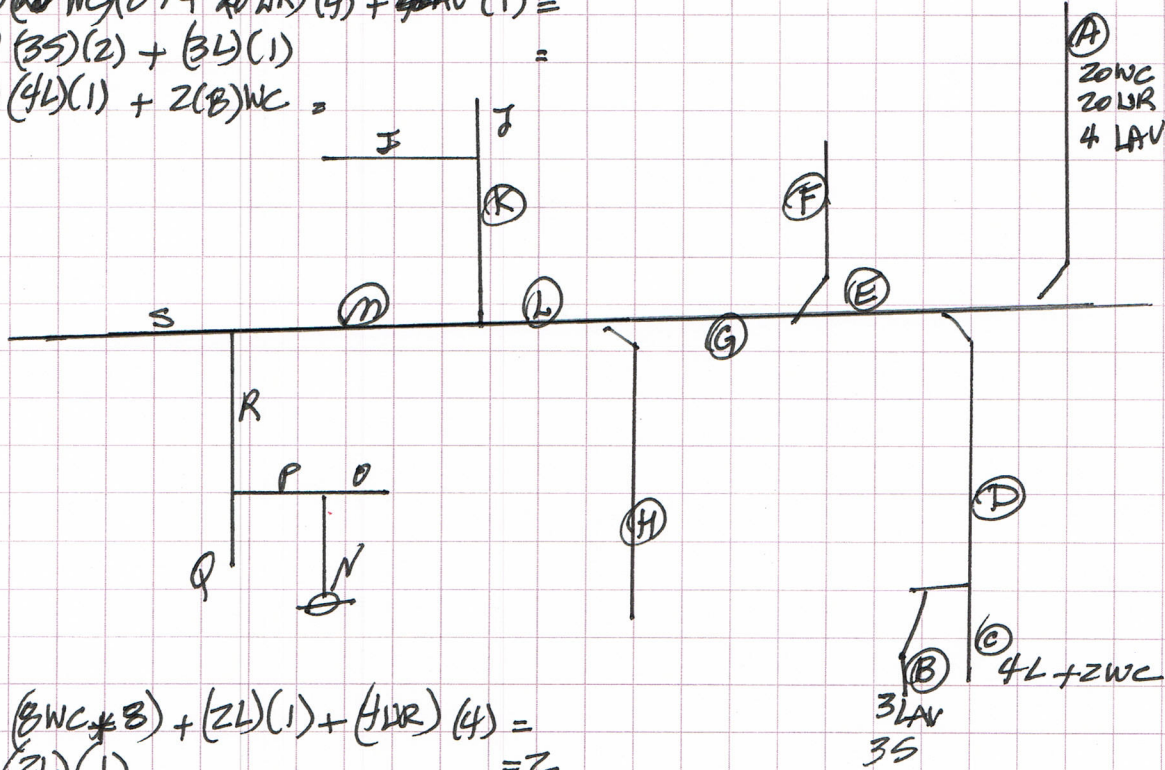
WATER HAMMER:
A SYMPTOM OF
HYDRAULIC SHOCK

HYDRAULIC SHOCK: SUDDEN & RAPID CHANGE IN VELOCITY
CAUSES: QUICK CLOSING VALVE



HOUSE DRAINAGE

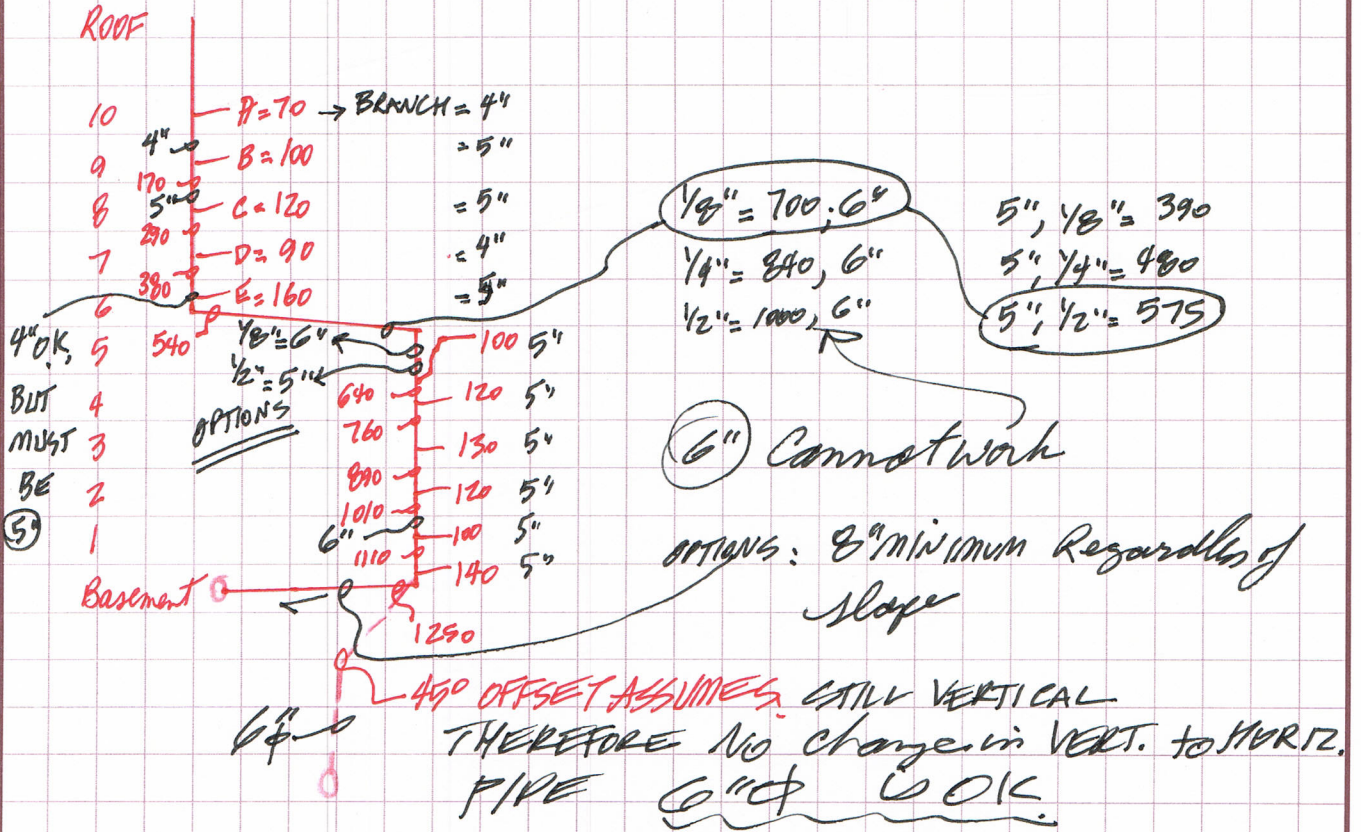
$(A) (20 WC)(8) + (20 UR)(4) + (4 LAV)(1) =$
 $(B) (35)(2) + (3L)(1) =$
 $(C) (4L)(1) + 2(B)WC =$



$(F) (8WC)(8) + (2L)(1) + (4UR)(4) =$
 $(H) (2L)(1) = 2$
 $(N) CLEAN OUT$
 $(D) (3BT)(2) + (3SH)(2) + (2WC)(8) =$
 $(J) (2BT)(3) + (2L)(2) =$
 $(I) (3WC)(8) + (2SK)(2) =$
 $(Q) 8(3WC) + (2SK) + (2L)(2) =$



STACK SIZING



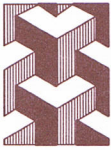
HOUSE DRAIN SIZING

1/2 CAPACITY TO 3/4 MAX. (TO PREVENT FLUCTUATIONS)

1/4" / FE FOR < 3" φ, & 1/8" > 3" φ O.K. 1/16" / FE FOR 6" φ < O.K.

	1/16" / FE	1/8" / FE	1/4"	1/2"
2" φ	1.02	1.44	2.03	2.88
3	1.24	1.76	2.49	3.53
4	1.44	2.03	2.88	4.07
5	1.61	2.28	3.53	4.56
6	1.76	2.49	4.07	5.0
8	2.03	2.88	4.23	5.75
10	2.28	3.23	4.56	6.44

SUMP PUMP @ 200 GPM =
2 x 200 = 400 FL.



FIXTURES

F. DRAIN SIZE
 BASED ON MIN TRAP SIZE

SANITARY FIXTURE UNIT (FU)

- ROY HUNTER BMS (1990)
- UNITS ASSIGNED TO DIFFERENT FIXTURES (1923)
- BASED ON PROBABILITY OF USE BASE ON CUMULATIVE F.U.'S (NOT GPM)
- 2 F.U. = 7.5 GPM/FS FACTOR = TOTAL GPM OF FIXTURE / 7.5 GAL/FS = FLOWRATE (??)
- PRIMARY REASON TO CUMULATIVE LOADING IN F.U.'S

STACK SIZING IN FU $q = 27.8 v^{5/3} d^{18/3}$
 MAX. FU FOR STACKS

PIPE SIZE	10 FU (3 STORIES OR LESS)	24 FU (3 STORIES)	TOTAL DISCHARGE 1 BRANCH G
2 1/2"	20	42	9
3"	30*	60*	16+
4"	240	500	90
5"	540	1100	200
6"	960	1900	350
8"	2200	3600	600
10"	3800	5600	1000
12"	6000	8400	1500

MAX FU	SANITARY BRANCHES
1 1/2"	F.U. 3
2"	6
2 1/2"	12
3"	20* < 2 W.C. MAX.
4"	160
5"	360
6"	620
8"	1400

* NOT MORE THAN 6 W.C.

+ NOT MORE THAN 2 W.C.

$q = v = 27.8 v^{5/3} d^{18/3} = 27.8 (7/24)^{5/3} (4)^{18/3} = 1456 \text{ GPM}$

MAX. LOADING = 1456 GPM, $v = 7/24$, > 3 STORIES, 4", 500 FU

MAX. F.U. SANITARY BUILDINGS & RENOVTS FROM STACKS

PIPE Ø	SLOPE 1/8" PER FT		
	1/8"	1/4"	1/2"
2"	-	21	26
2 1/2"	-	24	31
3"	20	27	36
4"	180	216	250
5"	390	480	575
6"	700	840	1000
8"	1600	1920	2300
10"	2900	3500	4200
12"	4600	5100	6700
15"	8300	10100	12000

2 F.U. = 1 GPM

Acknowledgments

The American Society of Plumbing Engineers gratefully acknowledges the contribution of Alfred Steele, P.E., CIPE, the author of the first Certified in Plumbing Design Examination Review Manual. Mr. Steele's original work forms the backbone upon which the ASPE CPD Review Manual Committee developed this revised manual.

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Program Development

The Certified in Plumbing Design (CPD) program is an international certification program for engineers and designers of plumbing systems. Completion of the CPD program and examination confers upon the successful candidate the designation Certified in Plumbing Design, or CPD. The certification program provides the profession, the plumbing industry, and the general public with a single, comprehensive qualification of professional competence for engineers and designers of plumbing systems. The CPD is the only international credential program in the plumbing engineering field. It sets the standards for leadership within the industry and provides formal recognition of outstanding professionals with advanced skills in the design and specification of plumbing systems.

PROGRAM OBJECTIVES

The CPD program was established with five primary objectives:

1. Provide a standard of professional competence for the practice of plumbing engineering.
2. Identify and recognize those individuals who successfully complete the certification examination, thereby demonstrating their acquired knowledge and abilities in the field of plumbing engineering.
3. Encourage plumbing engineers to participate in a continuing program of professional development.
4. Provide a standard for educational programs in plumbing engineering and encourage implementation of such programs.
5. Enhance the status of plumbing engineering as a unique discipline and profession by demonstrating that a realistic standard of professional competence can be clearly defined.

WHO IS ELIGIBLE?

To be eligible to take the CPD examination, a candidate must possess a minimum of four (4) years of practical experience in a position of responsibility for the design of plumbing systems and possess a baccalaureate degree in a field related to engineering. In lieu of an accredited degree, a candidate may substitute up to an additional four (4) years of practical experience in the design of plumbing systems [for a total of eight (8) years] or be granted a credit of one-half year of practical experience for each one (1) full year of education in an accredited curriculum related to plumbing engineering.

THE CPD EXAMINATION

The Certified in Plumbing Design Examination is offered annually in electronic digital form only, available at more than 200 testing sites around the country. The test specifications for the examination were developed by ASPE's Certification Committee with the help of an independent testing and certification service organization, using information derived from a job analysis. The test specifications and content reflect the knowledge, skills, and problem-solving experience essential to performing the job of a plumbing engineer.

Test Content

The Certified in Plumbing Design Examination consists of 100 multiple-choice questions. The questions in the CPD examination are linked to five broad task statements that describe the job dimensions of a plumbing engineer. These task statements are:

Task 1 and Task 2: Gathering Information and Administration — The plumbing engineer identifies the scope of work, existing physical conditions, and project team contacts; determines applicable requirements of authorities having jurisdiction, utility availability, and budgetary constraints; prepares and monitors work plans and schedules; and coordinates work with other members of the professional design team (e.g., HVAC, electrical, etc.).

Task 3: Design — The plumbing engineer identifies the required systems; establishes the design criteria for each system; designs each system; and coordinates the systems with all other building elements.

Task 4: Specifications — The plumbing engineer determines the format and coordinates it with the design; describes the systems to be used; and coordinates plumbing specifications with all other specifications.

Task 5: Construction Services — The plumbing engineer reviews submittals for compliance with contract documents; reviews the installation for compliance with contract documents; and witnesses system test(s).

To receive more information on the CPD exam, visit ASPE.org.